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(54) **PHOTOCATALYST COMPOUND AND PROCESS FOR PRODUCTION THEREOF**
PHOTOKATALYSATOR UND VERFAHREN ZUR HERSTELLUNG
COMPOSE PHOTOCATALYSEUR ET SON PROCEDE DE PRODUCTION

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Description

TECHNICAL FIELD

5 [0001] The present invention relates to a photocatalyst compound and to a process for production thereof.

BACKGROUND ART

[0002] Photocatalysis is known and has application in the treatment of fluids such as water containing pollutants.

10 [0003] Conventionally, a photocatalyst such as titanium dioxide (TiO₂) is added to the fluid to be treated to form a slurry. The slurry is then exposed to electromagnetic radiation which results in catalytic destruction or decomposition of the pollutants in the fluid. For TiO₂, radiation having a wavelength of less than or equal to about 380 nm results in catalytic destruction or decomposition of the pollutants in the fluid.

15 [0004] It is known in the art to load TiO₂ on a support to facilitate recovery of the TiO₂ in a specific place. However, as is known in the art, TiO₂ is a relatively poor adsorber of, inter alia, organic compounds and there has been little or no attention given to this in the art.

[0005] Indeed, much of the prior art has focused on methods of immobilizing the photocatalyst TiO₂ directly on to the support material. Generally, this technique involves thermal fusing of TiO₂ to a support material such as silica gel, etched glass beads, interior of glass tubes, Teflon™ tubing, woven glass mesh, sand and the like. See, for example,
20 any of the following prior art references:

1. Serpone et al., *Solar Energy Mater.* **14**, 121 (1986),
2. Matthews et al., *Anal. Chim. Acta.* **223**, 171 (1990),
3. Matthews, *Solar Energy Mater.* **38**, 405 (1987),
- 25 4. United States patent 5,182,030 (Crittenden et al.),
5. Australian patent application PH7074 (Matthews),
6. Stakheev et al., *J. Phys. Chem.* **97**, 5668 (1993),
7. Matthews, *Wat. Res.* **25**, 1169 (1991),
8. Yoneyana et al., *J. Phys. Chem.* **93** 4833 (1989),
- 30 9. Yamanaka et al., *Mater. Chem. Phys.* **17**, 87 (1987),
10. Minero et al., *Langmuir* **8**, 481 (1992), and
11. United States patent 4,495,041 (Goldstein).

35 [0006] While there appears to exist a commercial interest in TiO₂-based photocatalysis for the destruction or decomposition of pollutants in water, the known systems suffer from a number of disadvantages.

[0007] Specifically, a disadvantage of the work done to date is that, with most of the supported TiO₂ photocatalysts, there is a drop-off in the photoactivity of the photocatalysts compared to the photoactivity of unsupported TiO₂ photocatalyst.

40 [0008] Yet another disadvantage is that, with most of the prior art supported TiO₂ photocatalysts, there is a drop-off in the adsorption of pollutants by the photocatalysts compared to the adsorption characteristics of the support material, per se, due to the unfavourable adsorption characteristics of TiO₂.

[0009] It would be desirable to have a photocatalyst compound alleviate at least one of the above-identified disadvantages of the prior art.

45 DISCLOSURE OF THE INVENTION

[0010] It is an object of the present invention to provide a novel photocatalyst compound which obviates or mitigates at least one of the above-mentioned disadvantages of the prior art.

[0011] It is another object of the present invention to provide a novel process for producing a photocatalyst compound.

50 [0012] Accordingly, in one of its aspects, the present invention provides a photocatalyst compound comprising: (i) a photocatalyst selected from the group consisting of TiO₂, WO₃ and mixtures thereof, the photocatalyst being substantially free of sharp, narrow band X-ray reflections at angles corresponding those of crystalline TiO₂, WO₃ and mixtures thereof, and (ii) a porous, crystalline, adsorbent support material.

55 [0013] In another of its aspects, the present invention provides a process for producing a photocatalyst compound comprising the steps of:

- (i) hydrolysing a non-ionic titanium compound to produce a colloidal suspension having an average particle size of less than about 250Å;

- (ii) contacting a porous, crystalline, adsorbent support material with the colloidal suspension to produce an impregnated support; and
 (iii) calcining the impregnated support to produce a photocatalyst compound comprising a TiO_2 photocatalyst, the photocatalyst being substantially free of sharp, narrow band X-ray reflections at angles corresponding those of crystalline TiO_2 .

BRIEF DESCRIPTION OF THE DRAWINGS

[0014] Embodiments of the present invention will be described with reference to the accompanying drawings, in which:

- Figure 1 illustrates X-ray diffraction patterns for a number of unsupported TiO_2 photocatalysts;
 Figure 2(a) illustrates X-ray diffraction patterns for various photocatalyst compounds based on TiO_2 and ZSM5 zeolite;
 Figure 2(b) illustrates X-ray diffraction patterns for various photocatalyst compounds based on TiO_2 and Zeolite A;
 Figure 3(a) illustrates X-ray diffraction patterns for various photocatalyst based on TiO_2 and alumina;
 Figure 3(b) illustrates X-ray diffraction patterns for various photocatalyst based on TiO_2 and silica;
 Figure 4 illustrates various Raman spectra for TiO_2 photocatalyst and photocatalyst compounds based on TiO_2 /alumina and TiO_2 /silica;
 Figure 5 illustrates Raman spectra for ZSM5 zeolite and various photocatalysts based on TiO_2 and ZSM5 zeolite;
 Figure 6 illustrates Raman spectra of Zeolite A and various photocatalyst compounds based on TiO_2 and Zeolite A;
 Figure 7 illustrates the photoactivity of two TiO_2 photocatalysts;
 Figure 8 illustrates the photoactivity of various photocatalyst compounds based on TiO_2 /silica and TiO_2 /alumina;
 Figure 9 illustrates the photoactivity of various photocatalysts compounds based on TiO_2 and Zeolite A with and without the use of a UV cut-off filter during illumination;
 Figure 10 illustrates a photoactivity comparison between a photocatalyst based on TiO_2 /ZSM5 and another photocatalyst compound based on TiO_2 /Zeolite A in the photooxidation of 4-chlorophenol;
 Figure 11 illustrates a time profile of acetophenone adsorption on ZSM5 under dark conditions; and
 Figure 12 illustrates the effect of zeolite crystallinity on the photoactivity in acetophenone oxidation of a photocatalyst compound based on TiO_2 and Zeolite A.

BEST MODE FOR CARRYING OUT THE INVENTION

[0015] Thus, in one of its aspects, the present invention relates to a photocatalyst compound comprising (i) a photocatalyst selected from the group comprising TiO_2 , WO_3 and mixtures thereof wherein the photocatalyst does not exhibit sharp, narrow band X-ray reflections at angles corresponding those of crystalline TiO_2 , WO_3 and mixtures thereof, and (ii) a porous, crystalline, adsorbent support material.

[0016] The photocatalyst is TiO_2 , WO_3 or a mixture thereof which, using currently available analytical techniques, could be classified as "non-crystalline". As used herein, the term "non-crystalline", when used in regard to TiO_2 , WO_3 or mixtures thereof, is intended to connote that the material in question does not exhibit sharp, narrow band X-ray reflection at angles corresponding to those of crystalline TiO_2 , WO_3 and mixtures thereof. Thus, the photocatalyst useful in the present photocatalyst compound can be considered amorphous and free of long range order. For example, in the case of TiO_2 , the present photocatalyst compound comprises TiO_2 which does not exhibit the sharp narrow band X-ray reflections at angles where such reflections are characteristic of the presence of the anatase (2 θ of approximately 25.2) crystalline form of TiO_2 . Further, the characteristic X-ray reflections normally seen for the rutile (2 θ of approximately 27.3) or brookite crystalline (2 θ of approximately 30.8) forms of TiO_2 are not apparent in the present photocatalytic compounds.

[0017] The Raman spectra of present photocatalyst compounds is further characteristic of the presence of TiO_2 , WO_3 or mixtures thereof in an amorphous state. The Raman spectra of, *inter alia*, crystalline TiO_2 and WO_3 are discussed in "Spectroscopic Characterization of Supported Metal Oxide Catalysts" by M.A. Vuurman (1992, PhD research thesis conducted at the University of Amsterdam). Specifically, with reference to Chapter 6 of Vuurman, Figure 5 illustrates the Raman spectra for various loadings of WO_3 on alumina. Vuurman teaches (see page 97) that crystalline WO_3 particles have characteristic or "major" bands at 808, 711, 321 and 273 cm^{-1} . With further reference to Chapter 6 of Vuurman, Figure 6 illustrates the Raman spectra for various loading levels of TiO_2 on alumina. Vuurman teaches (see page 100) that crystalline TiO_2 particles have characteristic or "major" bands at 643, 520, 394 and 144 cm^{-1} . As discussed above, the present photocatalyst compounds comprise TiO_2 , WO_3 or mixtures thereof in an amorphous state. In such a state, the TiO_2 , WO_3 or mixtures thereof comprised in the present photocatalyst compounds, particularly give rise to Raman spectra which do not exhibit such characteristic or "major" bands.

[0018] In the present photocatalyst compounds, the photocatalyst (i.e. TiO_2 , WO_3 or mixtures thereof) forms a very thin amorphous layer which substantially completely covers the external surface of the adsorbent support material. This feature is particularly prevalent at relatively low loading levels of the TiO_2 , WO_3 or mixtures thereof (e.g. less than about 10% by weight of the photocatalyst compound) and is believed to be at least partially responsible for the enhanced photoactivity of this preferred subset of the present photocatalyst compounds.

[0019] The adsorbent support material suitable for use in the present photocatalyst compounds is porous and crystalline. Preferably, the support material has an average pore size in the range of from 5Å to 15Å, preferably from 7Å to 12Å.

[0020] The crystallinity of the adsorbent support material is an important feature. Specifically, the adsorbent support material should have a crystallinity of at least 50%, more preferably at least 60%, even more preferably at least 70%, most preferably at least 85%. The crystallinity of the support material can be readily determined by a person of skill in the art, for example, by means of comparison of the intensity of X-ray diffraction reflections for a given adsorbent support material with that of a crystalline material derived by a standard preparation.

[0021] Preferably, the adsorbent support material is zeolite (e.g. Zeolite A), more preferably a hydrophobic zeolite comprising a relatively high content of silicon, most preferably a silicon to aluminum weight ratio of from 10:1 to 100:1. Non-limiting examples of zeolites which are useful in the present invention may be selected from the group consisting of ZSM5, Zeolite A and mixtures thereof. As is known in the art, for a given zeolite material, there is some latitude to vary the silicon to aluminum weight ratio. It is contemplated that this latitude can be used to modify other zeolites such as other ZSM zeolites, Zeolite Y and Zeolite X to be useful in the present photocatalyst compounds.

[0022] While zeolites are the preferred choice for use as the adsorbent support material in the present photocatalyst compounds, non-zeolite materials may also be used. A preferred class of such materials is molecular sieves, more preferably hydrophobic molecular sieves. Non-limiting examples of suitable molecular sieves include titanium silicates (e.g. TS1), aluminum phosphates (also known as ALPO's) and members of the MCM family (e.g. MCM-10). Of course it is important that the zeolite chosen be of a crystalline nature as discussed hereinabove.

[0023] A portion of the TiO_2 and/or WO_3 be substituted with at least one transition metal of the Periodic Table. Preferably, the substitution will be up to 5% by weight, more preferably up to 2% by weight, of the photocatalyst compound.

[0024] More preferably, the transition metal is selected from the fourth period of the Periodic Table. Most preferably, the transition metal is selected from the group consisting of iron, vanadium, chromium and mixtures thereof. The preferred photocatalyst to be used in the photocatalyst compound of the present invention is substantially non-crystalline TiO_2 . While, in broad terms, the loading of TiO_2 in the photocatalyst compound is not generally restricted, the present inventors have discovered a particularly useful class of photocatalyst compounds which have a characteristic loading of the substantially non-crystalline TiO_2 in the range of from 0.5% to 10%, more preferably from 2% to 9%, most preferably from 2% to 6%, by weight of the photocatalyst compound. This class of photocatalyst compounds has been surprising and unexpectedly found to have enhanced specific activity compared to photocatalyst compounds which employ one or more of the following: (i) more than 10% by weight of TiO_2 , (ii) unsupported crystalline TiO_2 and (iii) photocatalysts supported on non-crystalline adsorbent support materials (e.g. various aluminas and silicas).

[0025] As discussed hereinabove, an aspect of the present invention a process for producing a photocatalyst compound comprising the steps of:

(i) hydrolysing a non-ionic titanium compound to produce a colloidal suspension having an average particle size of less than 250Å;

(ii) contacting a porous, crystalline, adsorbent support material with the colloidal suspension to produce an impregnated support; and

(iii) calcining the impregnated support to produce a photocatalyst compound comprising a TiO_2 photocatalyst, the photocatalyst being substantially free of sharp, narrow band X-ray reflections at angles corresponding those of crystalline TiO_2 .

[0026] Thus, Step (i) of the process involves starting with a non-ionic titanium compound, a tungsten compound or a mixtures thereof. Preferably, the starting material is one a non-ionic titanium compound and a tungsten compound. Preferably, the non-ionic titanium compound is selected from the group consisting of TiCl_4 , $\text{Ti}(\text{OR})_4$ and mixtures thereof, wherein R is a C_1 - C_{10} alkyl group. The preferred group for R is propyl. The starting material is subjected to hydrolysis to produce a colloidal suspension having an average particle size of less than about 250Å. If the average particle size exceeds about 250Å, there is a significant likelihood of the occurrence of agglomerations of the photocatalyst. Preferably the starting material is initially dissolved in a suitable water-miscible organic solvent prior to hydrolysis. This may be achieved by, for example, slow addition to the starting material of a stoichiometric amount of water over a period of time which is longer than the rate of the hydrolysis reaction. This can be done by controlling addition of the water to a rate which is slow enough to ensure that each addition of water leads to hydrolysis. The result is a colloidal suspension having an average particle size of less than 250Å, preferably in the range of from 20Å to 100Å, more preferably in the

range of from 20Å to 75Å. This suspension may be considered as sol. More information on the general preparation of sols may be found in *J. Membrane Sci.*, 1988, 39, 243 (Anderson et al.).

[0027] In Step (ii) of the process, the colloidal suspension is used to impregnate the adsorbent support material. Generally, this involves contacting the adsorbent support material with the colloidal suspension produced in Step (i) of the process. Preferably, the contacting is done with mixing. While the duration of contact between the colloidal suspension and the adsorbent support material is not particularly restricted, it is preferred that duration of contact be at least about 1 hour. After the colloidal suspension and the adsorbent support material have been contacted for a period sufficient to effect impregnation of the latter, the impregnated support material may be isolated by any conventional physical separation technique (e.g. gravity filtration and the like). Thereafter, it is preferred to dry the impregnated support material. This can be done by air drying at a temperature in the range of from 20° to 150°C.

[0028] In Step (iii) of the process, the impregnated support material is calcined to produce a photocatalyst compound comprising a photocatalyst selected from the group consisting of TiO₂, WO₃ and mixtures thereof, the photocatalyst being substantially free of sharp, narrow band X-ray reflections at angles corresponding those of crystalline TiO₂, WO₃ and mixtures thereof. The conditions of calcination are not particularly restricted and are generally within the purview of a person skill in the art. Preferably, calcination is conducted at a temperature in the range of from 250° to 500°C for a period of at least 12 hours.

[0029] When it is desired to produce a photocatalyst compound loaded with WO₃, it is preferred to contact the support material with a tungstate compound, preferably a metatungstate compound, more preferably ammonium metatungstate ((NH₄)₆H₂W₁₂O₄₀). This results in impregnation of the support material, which can then be separated, dried, and calcined as described above.

[0030] The present photocatalyst compound is useful in the treatment fluids containing, *inter alia*, organic pollutants. Generally, the photocatalyst compound can be used to catalyze photooxidation of the pollutants. This can be done by disposing the photocatalyst compound in the fluid to be treated and irradiating the fluid with radiation of a suitable wavelength. The treatment process can be continuous or batch-wise. The design of a suitable fluid treatment system incorporating the present photocatalyst compound is within the purview of those of skill in the art.

[0031] Embodiments of the present invention will be described with reference to the following Examples which should not be construed as limiting the invention.

EXAMPLE 1

[0032] A reactant composition comprising 200 mL, 1 mL nitric acid and 28.1 g titanium (IV) tetraisopropoxide (97% pure, Aldrich) was dissolved in 10 mL ethanol. The resulting slurry was peptized for 8 hours to produce a TiO₂ sol. More information on this procedure may be obtained *J. Membrane Sci.*, 1988, 39, 243 (Anderson et al.).

[0033] The TiO₂ photocatalyst was supported on the following materials:

Designation	Support Material
A	ZSM5 zeolite
B	Zeolite A
C	Alumina
D	Silica

[0034] The ZSM5 zeolite was synthesized under hydrothermal conditions in a Teflon™-lined autoclave using the procedure described in United States patent 3,702,866 (Arganer et al.). The molar chemical composition of the resulting gel was:



(TPAB = tetrapropylammoniumbromide). Crystallization was done statically at 175°C over a period of 10 days. The resulting crystalline solid was filtered, washed with water, dried at 120°C overnight and calcined at 550°C for a period of 12 hours in dry air. The structure of the ZSM5 zeolite was confirmed by a comparative analysis with the known structure of the zeolite - see "Collection of Simulated XRD Powder Patterns for Zeolites. A Special Issue of Zeolites", *Int. J. Molecular Sieves*, 1990, 10(5), 323-520 (Ballmoos et al.).

[0035] Zeolite A was obtained from Aldrich. This zeolite had the following chemical composition:



and was characterized by an average particle size of 3-5 μm .

[0036] The alumina was an acidic type obtained from BDH.

[0037] The silica was Silica Gel 100 obtained from EM Science. The silica gel had particle diameters ranging from 0.063 to 0.200 mm, a mean pore diameter of 100Å, a specific surface area of 420 m^2/g and a pore volume of 1.05 mL/g. The pH of a 10% aqueous suspension of the silica gel was determined to be 7.0-7.5.

[0038] The general technique for loading the TiO_2 on to the support material was as follows. A suspension of 4.5 g of the support material saturated with 10 mL water was mixed for $\frac{1}{2}$ hour. The suspension was then mixed, with stirring, with 5 mL of the TiO_2 sol. The mixture was dried by evaporation at 50°C over a period of 2 to 3 hours. Thereafter, the dried mixture was heated at 120° overnight and calcined at 450°C for a period of 11-12 hours. Using this general technique, various Samples of photocatalyst compounds were produced with a varying content of TiO_2 on each support material, as indicated in Tables 1-4 (A, B, C and D have the designations discussed above).

TABLE 1

Sample	TiO_2 (% by weight)
A-1	0
A-2	1.4
A-3	5.0
A-4	9.7
A-5	14.3
A-6	18.6

TABLE 2

Sample	TiO_2 (% by weight)
B-1	0
B-2	1.5
B-3	3.8
B-4	9.9
B-5	14.6
B-6	21.0
B-7	39.5

TABLE 3

Sample	TiO_2 (% by weight)
C-1	0
C-2	1.8
C-3	3.3
C-4	7.9
C-5	13.5
C-6	21.2
C-7	34.2

TABLE 4

Sample	TiO ₂ (% by weight)
D-1	0
D-2	2.1
D-3	5.9
D-4	19.6
D-5	24.4
D-6	34.5

[0039] As will be apparent to those of skill in the art, Samples C-1 through C-7 (alumina support material) and D-1 through D-6 (silica support material) are for comparative purposes only and thus, are outside the scope of the present invention.

[0040] Also for comparative purposes, a sample of TiO₂ was obtained from Degussa Corporation under the trade-name P25 and designated herein as CON-1. For further comparative purposes, an unsupported TiO₂ photocatalyst was produced by evaporation of the solvent in the TiO₂ sol (described above) to produce a white powder. The white powder was then heated at 120°C overnight. The dried product was designated CON-3. The dried product was then calcined at 450°C for a period of 11-12 hours to produce a calcined product which was designated CON-2. These various unsupported TiO₂ photocatalysts are referred to in Figure 1.

[0041] X-ray powder diffraction patterns were recorded using Cu K α radiation ($\lambda = 1.54059 \text{ \AA}$) on a Scintag XDS 2000 X-ray diffractometer. Diffraction patterns were taken over the 2θ range of 5° to 50° and the results were treated with the Jade program for XRD pattern-processing (Materials Data, Inc.) The crystallinity of Zeolite A was determined by measuring the total peak area under eight main peaks over the 2θ range of 5° to 35°.

[0042] With reference to Figure 1, it will be apparent to those of skill in the art that the principal constituent of each of CON-1, CON-2 and CON-3 is the anatase (A) crystalline form of TiO₂. The rutile (R) and brookite (B) crystalline forms of TiO₂ are present at in relatively minor amounts.

[0043] With reference to Figure 3, it will be apparent to those of skill in the art that the characteristic anatase-, rutile- and brookite-attributable peaks found in Figure 1 are also present in Samples produced using alumina (Figure 3(a)) and silica (Figure 3(b)) as the support material. This is strong evidence that use of alumina and silica as a support material results in loading of TiO₂ having relatively high crystallinity.

[0044] In contrast, with reference to Figure 2, it will be apparent to those of skill in the art that the overriding feature of the pattern for each sample is the presence of TiO₂ which lacks the narrow, sharp characteristic anatase-, rutile- or brookite-attributable peaks found in Figure 1. This is especially true for those Samples having a TiO₂ loading level of less than about 10% by weight TiO₂ (i.e. A-1 through A-4 and B-1 through B-4). This is strong evidence that use of the chosen zeolites as a support material results in loading of TiO₂ lacking well formed TiO₂ phases (in other words, the TiO₂ is present in an amorphous or possibly microcrystalline form).

[0045] The crystallinity of various Samples was assessed calculating the ratio of peak area for peak positions chosen at 2θ values of 25.2, 27.3 and 30.8 for anatase (A), rutile (R) and brookite (B), respectively. The results are reported in Table 5 wherein the peak width reported was measured at half peak height of the anatase peak at a 2θ value of 25.2 and the ratio of peak area is reported as the ratio of the parameter for the given Sample to that of TiO₂ (CON-1) at a 2θ value of 25.2.

[0046] As reported in Table 5, the peak width for Sample B-7 and a Sample comprised of 36.4% by weight TiO₂ on ZSM5 was quite broad and weak. This led to the conclusion that the TiO₂ in each of these Samples was amorphous. In contrast, it was possible to conclude that the TiO₂ in Samples CON-1, CON-2, CON-3, C-7 (alumina support) and D-6 (silica support) was present predominantly in the anatase crystalline form. As will be demonstrated hereinbelow, the presence of this crystallinity in TiO₂ is associated with inferior photoactivity. Indeed, with reference to the final Sample reported in Table 5, it will be noted the narrow peak width remains notwithstanding the destruction of the crystallinity of the Sample. In contrast, the peak width for Sample B-7 and a Sample comprised of 36.4% by weight TiO₂ on ZSM5 was quite broad and weak. This leads to the conclusion that the interaction of the TiO₂ and zeolite in these Samples is different than that of a physical admixture of the TiO₂ and zeolite.

TABLE 5

Sample	Anatase (%)	Rutile (%)	Brook-kite (%)	Peak Width	Ratio of Peak Area
CON-3	96.6	-	3.4	1.51	33

TABLE 5 (continued)

Sample	Anatase (%)	Rutile (%)	Brook-kite (%)	Peak Width	Ratio of Peak Area
CON-2	88.6	7.6	3.8	0.38	90
CON-2	85.7	14.3	-	0.42	100
B-7	AM	AM	AM	~1.2	~18
36.4% TiO ₂ /ZSM5	AM	AM	AM	~0.9	~14
D-6	93.9	-	6.1	1.11	44
C-7	94.6	-	5.4	1.46	44
Mechanical Mixture ¹	-	-	-	0.40	68

¹Mechanically ground mixture of 56% CON-1 and zeolite

[0047] The Raman spectra of various Samples were obtained on a Jarrel-Ash Model 25-100 spectrometer interfaced to a microcomputer. The software on the microcomputer allowed for multiple scans. The Raman spectra are provided on Figures 4-6.

[0048] Figure 4 illustrates the Raman spectra for the following Samples: CON-1, C-1, C-2, C-3, D-1, D-2 and D-3. As will be apparent to those of skill in the art, the spectrum for CON-1 compares favourably with that reported in the literature (see, for example, *Applied Spectrosc.*, 1972, 26, 537 (Capwell et al.)). This spectrum indicates that TiO₂ is predominantly in the anatase crystalline form. As will be further apparent to those of skill in the art, the spectra for Samples C-1 through C-3 and D-1 through D-3 are in satisfactory agreement with assignment of the TiO₂ therein being predominately in the anatase crystalline form.

[0049] In Figure 5, there are illustrated various Raman spectra for unsupported and TiO₂ supported photocatalyst Samples based on a support material which is ZSM5 zeolite. As illustrated for a TiO₂ loading of less than 1.9% on ZSM5, a new band appears at 380cm⁻¹. This peak is distinct from the ZSM5 band at 374cm⁻¹ and its intensity is greater than the 636cm⁻¹ band normally attributed to the presence of anatase crystalline form of TiO₂. As the TiO₂ loading increases, the new peak shifts toward the 396cm⁻¹ frequency which is typically characteristic of anatase crystalline form of TiO₂. Concurrently, the ratio of the peak intensity at 638cm⁻¹ to that at 380-396cm⁻¹ increases. At 9.7% by weight TiO₂ loading, the spectrum begins to approach that of TiO₂ powder.

[0050] Figure 6 illustrates Raman spectra of unsupported and TiO₂ supported photocatalyst based on a support material which is Zeolite A. The various loadings of TiO₂ are shown in Figure 6. These spectra are very similar to those provided in Figure 5 and serve to distinguish the zeolite loaded TiO₂ photocatalyst from photocatalysts loaded on alumina and silica (Figure 4).

EXAMPLE 2

[0051] In this Example, the photocatalytic activity of various of the Samples referred to in Example 1 was assessed. The two substrates chosen for testing photocatalytic activity were: acetophenone and 4-chlorophenol. Photocatalytic activity was evaluated by measuring the loss of the substrates during controlled experiments.

[0052] The protocol followed in evaluation of photocatalytic activity was as follows. Prior to commencing illumination, a suspension containing 0.5 grams photocatalyst and 100 mL of approximately 50 ppm acetophenone or 4-chlorophenol was stirred continuously for one hour. The concentration of the substrate in bulk solution at this point was used as the initial value for further kinetic treatment of the photodegradation processes. The decrease in concentration of the substrate in one hour was used for calculation of the extent of substrate adsorption on the specific photocatalyst.

[0053] The reactor used was a glass vessel with a flat port window for illumination. The reactor was cooled by water circulation to 20°C during each experiment. The irradiation source was a 200W Xenon lamp enclosed in a A1010 lamp housing from PTI and powered to 185 mW with a 250LPS power supply from PTI. A water cell was used as an infrared filter to filter out heat. A 320 nm cut-off filter was placed at the end of the water filter for each experiment with acetophenone and a 350 nm cut-off filter was used for experiments using 4-chlorophenol as the substrate.

[0054] Total irradiation time was 3 hours for each experiment. Oxygen was not added to the reaction vessel nor was ambient air removed. At each interval of 15-20 minutes, a 2 mL aliquot of sample was withdrawn by syringe from the irradiated suspension and filtered through a suitable filter membrane. The filtrate was analyzed for acetophenone using a HP 5880 GC instrument with a flame ionization detector and a copper coil column which was packed with 3% OB-225 on Chromosorb™. Analytical determination of 4-chlorophenol and intermediates in oxidation thereof were carried out using a Waters HPLC equipped with a UV-VIS detector and a reverse-phase C₁₈ column (MCH10 Varian Associates

Inc.). The eluants used comprised a mixture of water, acetonitrile and acetic acid (70:30:0.2 v/v) - see *Langmuir*, 1989, 5, 250 (Al-Ekabi et al.).

[0055] The photodegradation processes of acetophenone and 4-chlorophenol tended to follow pseudo-first order kinetics in the presence of the photocatalysts tested herein. The loss of the substrate was fitted to the corresponding logarithmic expression:

$$\text{Log } [C]_t = -k_{\text{app}} t + \text{Log } [C]_0$$

wherein $[C]_0$ and $[C]_t$ represent the concentration (ppm) of the substrate in solution at time = 0 and time = time of illumination, respectively, and k_{app} represents the apparent rate constant which is also referred to herein as "k".

[0056] No photodegradation of acetophenone or 4-chlorophenol was observed in the presence of any of the support materials (i.e. silica, alumina and the zeolites) when samples were illuminated at a wavelength longer than the longest band in the substrate spectrum ($\lambda > 320\text{nm}$ for acetophenone; $\lambda > 350\text{nm}$ for 4-chlorophenol). The support materials used in each were not observably photocatalytic. As indicated above, in all experiments with the TiO_2 photocatalysts where photodegradation of substrates was observed, the degradation kinetics were satisfactorily fit to a first order rate law. Consequently, relative reactivity was measured in terms of trends in the first order rate constant k_{app} , obtained under constant illumination as described above. Thus, an increase in k_{app} is indicative of an increase in photoactivity.

[0057] With reference to Figure 7, there is illustrated a graph of k versus TiO_2 concentration (mg/100 mL) for CON-1 (○) and CON-2 (●). As illustrated, the rate constant k increases with the concentration of TiO_2 but approaches a limit and does not increase further above about 1g/L. This behaviour has been observed in the art and is indicative that, with sufficient loading, all light is absorbed by TiO_2 and the further addition of catalysts does not increase reaction. As illustrated, CON-2 is less active as a photocatalyst than CON-1.

[0058] With reference to Figure 8, there is illustrated a plot of k versus % by weight TiO_2 for various samples of TiO_2 loaded onto silica (○) and TiO_2 loaded onto alumina (●). In the dark, prior to illumination, the acetophenone concentration decreases by 3% in the presence of 5.0 g/L of the silica supported catalyst. Dark adsorption of acetophenone on the alumina supported catalyst was not detectable under parallel conditions. As shown, at comparable total titanium loading (5 g/L of supported catalyst in Figure 8 corresponds to 0.5 g/L of TiO_2), the silica supported photocatalyst has the largest value of k amongst those materials tested in Figures 7 and 8, and thus is the most efficient.

[0059] With reference to Figure 9, there is illustrated a plot of k versus % by weight TiO_2 for a series of TiO_2 /zeolite A photocatalyst compounds without a UV cut-off filter used during illumination (○) and with a 320 nm cut-off filter used during illumination (□). The substrate used for oxidation was acetophenone. As illustrated, when a zeolite is employed as the support material, photoactivity is enhanced when compared to the photoactivity reported in Figures 7 and 8, especially at lower concentrations of TiO_2 . Similarly beneficial results were obtained when the substrate was changed to 4-chlorophenol as shown in Figure 10 wherein there is illustrated a plot of k versus % by weight TiO_2 for a series of TiO_2 /ZSM5 photocatalyst compounds (○) and TiO_2 /zeolite A (●) photocatalyst compounds.

[0060] With reference to Figure 11, there is illustrated a plot of substrate concentration versus time. Two substrates were used: a 200ppm acetophenone solution (○) and a 100ppm acetophenone solution (●). Thus, this study amounted to a time profile of acetophenone adsorption onto ZSM5 zeolite in dark condition for ZSM5 zeolite only. When the ZSM5 zeolite is loaded with TiO_2 as described above, there is no significant loss in the adsorption properties of the photocatalyst compound.

EXAMPLE 3

[0061] In this Example, the effect of crystallinity of the zeolite as a support material for the present photocatalyst compound is illustrated. The zeolite used in this Example was Zeolite A. A series of samples with a constant loading of TiO_2 and varying levels of crystallinity were produced via treatment of the photocatalyst with varying concentrations of nitric acid.

[0062] Zeolite crystallinity was calculated by determining the area under 8 principle XRD peaks of Zeolite A (2θ from 5° to 35°) compared to the non-acid-treated sample as a standard. The substrate used in this Example was acetophenone since it has a weak adsorption on Zeolite A. In the dark, acetophenone concentration in solution decreased by 2-4% in the presence of 5 g/L of the photocatalyst. There was no significant loss of adsorption on loss of crystallinity.

[0063] With reference to Figure 12, there is illustrated a plot of k versus % crystallinity of the support material in the photocatalyst. As illustrated, photoactivity increased markedly above approximately 50% crystallinity in the support material. This is a surprising and unexpected result.

Claims

1. A photocatalyst compound comprising: (i) a photocatalyst selected from the group consisting of TiO_2 , WO_3 and mixtures thereof, the photocatalyst being substantially free of sharp, narrow band X-ray reflections at angles corresponding those of crystalline TiO_2 , WO_3 and mixtures thereof, and (ii) a porous, crystalline, adsorbent support material.
2. The photocatalyst compound defined in claim 1, wherein the photocatalyst is TiO_2 .
3. The photocatalyst compound defined in any one of claims 1-2, wherein the support material has a crystallinity of at least 50%.
4. The photocatalyst compound defined in any one of claims 1-3, wherein the support material has an average pore size in the range of from 5Å to 15Å.
5. The photocatalyst compound defined in any one of claims 1-4, wherein support material is a hydrophobic zeolite comprising a silicon to aluminum weight ratio in the range of from 10:1 to 100:1.
6. The photocatalyst compound defined in any one of claims 1-5, wherein the support material is selected from the group consisting of ZSM5, Zeolite A and mixtures thereof.
7. The photocatalyst compound defined in any one of claims 1-6, wherein the photocatalyst further comprises up to 2% by weight of at least one transition metal selected from the Periodic Table.
8. The photocatalyst compound defined in any one of claims 1-7, wherein the TiO_2 is present in an amount of from 0.5% to 10% by weight of the photocatalyst compound.
9. A process for producing a photocatalyst compound comprising the steps of:
 - (i) hydrolysing a non-ionic titanium compound to produce a colloidal suspension having an average particle size of less than 250Å;
 - (ii) contacting a porous, crystalline, adsorbent support material with the colloidal suspension to produce an impregnated support; and
 - (iii) calcining the impregnated support to produce a photocatalyst compound comprising a TiO_2 photocatalyst, the photocatalyst being substantially free of sharp, narrow band X-ray reflections at angles corresponding those of crystalline TiO_2 .
10. The process defined in claim 10, wherein the non-ionic titanium compound is selected from the group consisting of TiCl_4 , $\text{Ti}(\text{OR})_4$ and mixtures thereof, wherein R is a C_1 - C_{10} alkyl group.
11. The process defined in claim 10, wherein R is propyl.
12. The process defined in any one of claims 9-11, wherein, prior to Step (i), the non-ionic titanium compound is dissolved in a water-miscible organic solvent.
13. The process defined in any one of claims 9-12, wherein the colloidal suspension has an average particle size in the range of from 20Å to 100Å.
14. The process defined in any one of claims 9-13, wherein Step (ii) further comprises air drying the impregnated support at a temperature in the range of from 20° to 150°C.
15. The process defined in any one of claims 9-14, wherein Step (iii) comprises calcining the impregnated support at a temperature in the range of from 250° to 500°C for a period of at least 12 hours.

Patentansprüche

1. Fotokatalysatorverbindung, welche enthält: (i) einen Fotokatalysator, der aus der Gruppe aus TiO_2 , WO_3 und Ge-

mischen daraus ausgewählt wird, wobei der Fotokatalysator im wesentlichen frei von scharfen und schmalbandigen Röntgenstrahl-Reflexionen unter Winkeln, die denen des kristallinen TiO_2 , WO_3 und Gemischen daraus entsprechen, ist, und (ii) ein poröses, kristallines, adsorbierendes Trägermaterial.

- 5 2. Die in Anspruch 1 dargestellte Fotokatalysatorverbindung, in der TiO_2 der Fotokatalysator ist.
3. Die in einem der Ansprüche 1 bis 2 dargestellte Fotokatalysatorverbindung, in der das Trägermaterial eine Kristallinität von mindestens 50 % aufweist.
- 10 4. Die in einem der Ansprüche 1 bis 3 dargestellte Fotokatalysatorverbindung, in der das Trägermaterial eine durchschnittliche Porengröße im Bereich von 5 Å bis 15 Å hat.
5. Die in einem der Ansprüche 1 bis 4 dargestellte Fotokatalysatorverbindung, in der das Trägermaterial ein hydrophober Zeolith ist, der ein Silizium/Aluminium-Gewichtsverhältnis im Bereich von 10 : 1 bis 100 : 1 hat.
- 15 6. Die in einem der Ansprüche 1 bis 5 dargestellte Fotokatalysatorverbindung, in der das Trägermaterial aus der Gruppe aus ZSMS, Zeolith A und Mischungen daraus ausgewählt wird.
7. Die in einem der Ansprüche 1 bis 6 dargestellte Fotokatalysatorverbindung, in der das Trägermaterial zusätzlich bis zu 2 Gew.-% von mindestens einem Übergangsmaterial aus der Tabelle des Periodensystems enthält.
- 20 8. Die in einem der Ansprüche 1 bis 7 dargestellte Fotokatalysatorverbindung, in der das TiO_2 in einer Menge von 0,5 bis 10 Gew.-% der Fotokatalysatorverbindung vorhanden ist.
- 25 9. Ein Verfahren zur Herstellung einer Fotokatalysatorverbindung, die die folgenden Schritte umfaßt:
 - (i) Hydrolisierung einer nicht-ionischen Titanverbindung, um eine kolloide Suspension zu erzeugen, die eine durchschnittliche Teilchengröße von weniger als 250 Å aufweist;
 - (ii) Kontaktieren eines porösen, kristallinen, adsorbierenden Trägermaterials mit der kolloiden Suspension, um einen imprägnierten Träger zu erzeugen; und
 - (iii) Kalzinieren des imprägnierten Trägers, um eine Fotokatalysatorverbindung zu erzeugen, die einen TiO_2 -Fotokatalysator enthält, wobei dieser Fotokatalysator im wesentlichen frei von scharfen und schmalbandigen Röntgenstrahl-Reflexionen unter Winkeln, die denen des kristallinen TiO_2 entsprechen, ist.
- 35 10. Das in Anspruch 10 dargestellte Verfahren, in welchem die nicht-ionische Titanverbindung aus der Gruppe TiCl_4 , $\text{Ti}(\text{OR})_4$ und Gemischen daraus ausgewählt wird, wobei R eine Alkylgruppe C_1 - C_{10} ist.
11. Das in Anspruch 10 dargestellte Verfahren, in welchem R ein Propyl ist.
- 40 12. Das in einem der Ansprüche 9 - 11 dargestellte Verfahren, in welchem vor dem Schritt (i) die nicht-ionische Titanverbindung in einem mit Wasser mischbaren organischen Lösungsmittel gelöst wird.
13. Das in einem der Ansprüche 9 - 12 dargestellte Verfahren, in welchem die kolloide Suspension eine durchschnittliche Teilchengröße im Bereich von 20 Å bis 100 Å hat.
- 45 14. Das in einem der Ansprüche 9 - 13 dargestellte Verfahren, in welchem der Schritt (ii) zusätzlich das Trocknen des imprägnierten Trägers mit Luft bei einer Temperatur im Bereich von 20 bis 150 °C umfaßt.
15. Das in einem der Ansprüche 9 - 14 dargestellte Verfahren, in welchem der Schritt (iii) das Kalzinieren des imprägnierten Trägers bei einer Temperatur im Bereich von 250 bis 500 °C über eine Zeitspanne von mindestens 12 Stunden umfaßt.
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Revendications

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1. Composé photocatalyseur contenant (i) un photocatalyseur sélectionné dans un groupe comprenant le TiO_2 , le WO_3 et des mélanges de ceux-ci, ce photocatalyseur étant sensiblement exempt de réflexions nettes de rayons X en bande étroite à des angles correspondant à ceux du TiO_2 , du WO_3 et de mélanges de ceux-ci, et (ii) un

matériau de support cristallin, poreux et adsorbant.

2. Composé photocatalyseur selon la revendication 1, caractérisé en ce que le photocatalyseur est le TiO_2 .
- 5 3. Composé photocatalyseur selon la revendication 1 ou 2, caractérisé en ce que le matériau de support présente une cristallinité de 50 % au moins.
4. Composé photocatalyseur selon l'une quelconque des revendications 1 à 3, caractérisé en ce que le matériau de support a une taille de pores moyenne de l'ordre de 5 Å à 15 Å.
- 10 5. Composé photocatalyseur selon l'une quelconque des revendications 1 à 4, caractérisé en ce que le matériau de support est une zéolite hydrophobe ayant un rapport de poids entre silicium et aluminium de l'ordre de 10:1 à 100:1.
6. Composé photocatalyseur selon l'une quelconque des revendications 1 à 5, caractérisé en ce que le matériau de support est sélectionné dans un groupe comprenant le ZSM5, la Zéolite A et des mélanges de ceux-ci.
- 15 7. Composé photocatalyseur selon l'une quelconque des revendications 1 à 6, caractérisé en ce que le photocatalyseur contient jusqu'à 2 % du poids d'au moins un métal de transition sélectionné dans la table de classification périodique.
- 20 8. Composé photocatalyseur selon l'une quelconque des revendications 1 à 7, caractérisé en ce que le TiO_2 représente de 0,5 % à 10 % du poids du composé photocatalyseur.
9. Procédé de production d'un composé photocatalyseur, comprenant les étapes de :
25 (i) hydrolyse d'un composé de titane non ionique en vue de produire une suspension colloïdale ayant une taille de particules moyenne inférieure à 250 Å ;
(ii) mise en contact d'un matériau de support poreux, cristallin et adsorbant avec la suspension colloïdale en vue de produire un support imprégné ; et
30 (iii) calcination du support imprégné en vue de produire un composé photocatalyseur contenant un photocatalyseur au TiO_2 , ce photocatalyseur étant sensiblement exempt de réflexions nettes des rayons X en bande étroite à des angles correspondant à ceux du TiO_2 cristallin.
10. Procédé selon la revendication 10, caractérisé en ce que le composé de titane non ionique est sélectionné dans le groupe comprenant le TiCl_4 , le $\text{Ti}(\text{OR})_4$ et des mélanges de ceux-ci, où R est un groupe alkyle C_1 - C_{10} .
- 35 11. Procédé selon la revendication 10, caractérisé en ce que R est du propyle.
12. Procédé selon l'une quelconque des revendications 9 à 11, caractérisé en ce qu'avant l'étape (i), le composé de titane non ionique est dissous dans un solvant organique miscible dans l'eau.
- 40 13. Procédé selon l'une quelconque des revendications 9 à 12, caractérisé en ce que la suspension colloïdale a une taille de particules moyenne de l'ordre de 20 Å à 100 Å.
14. Procédé selon l'une quelconque des revendications 9 à 13, caractérisé en ce que l'étape (ii) comprend en outre le séchage à l'air du support imprégné à une température comprise entre 20°C et 150°C.
- 45 15. Procédé selon l'une quelconque des revendications 9 à 14, caractérisé en ce que l'étape (iii) comprend la calcination du support imprégné à une température comprise entre 250°C et 500°C pendant au moins 12 heures.
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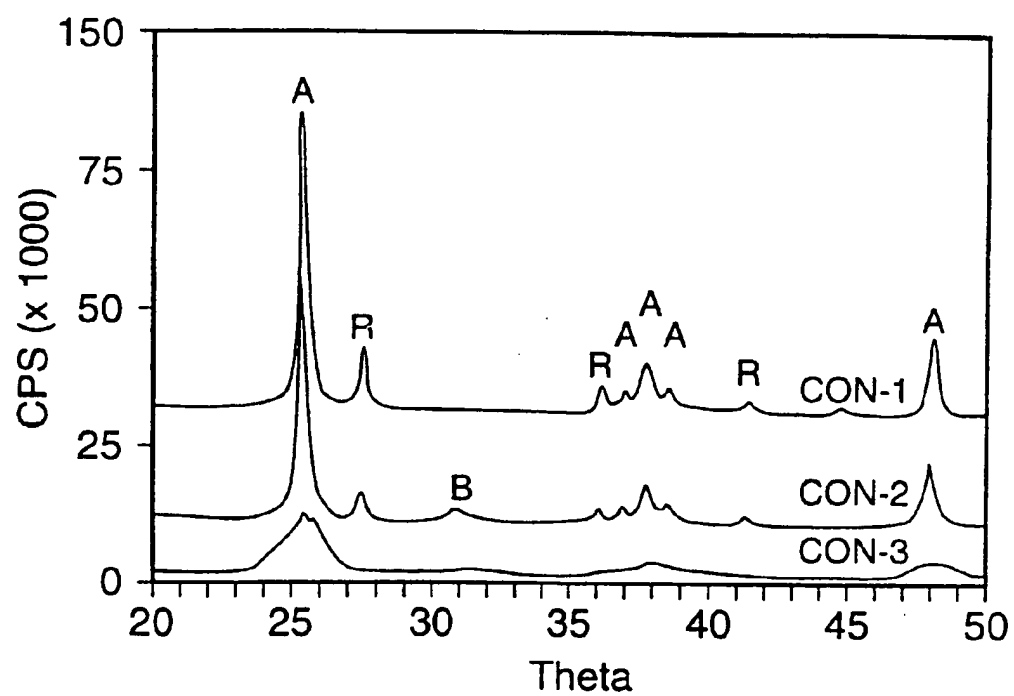
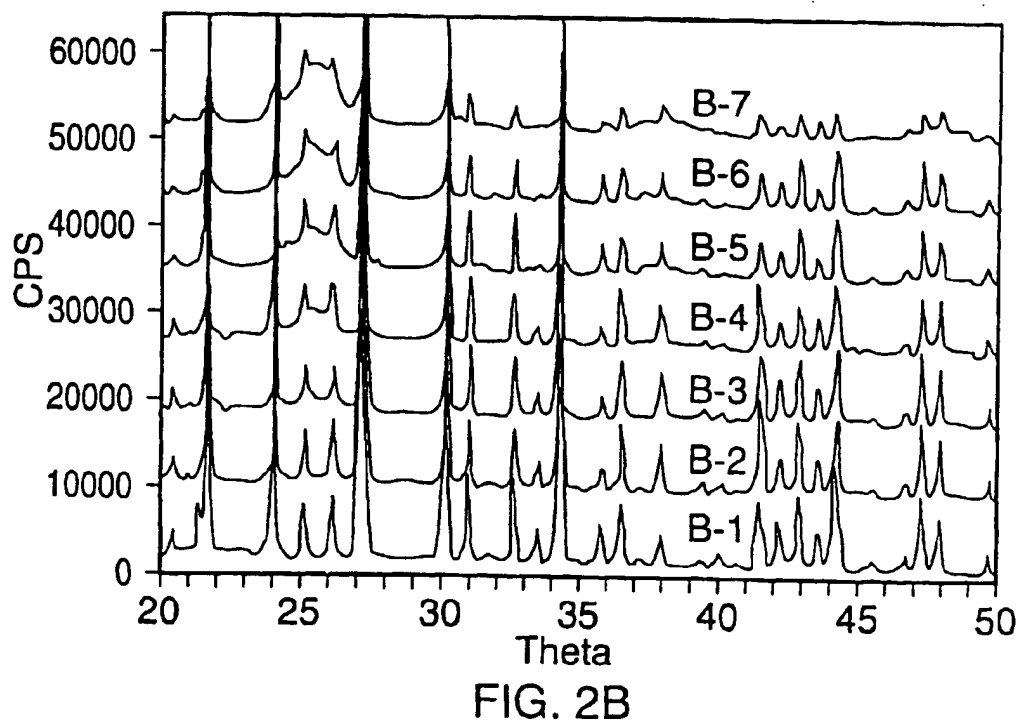
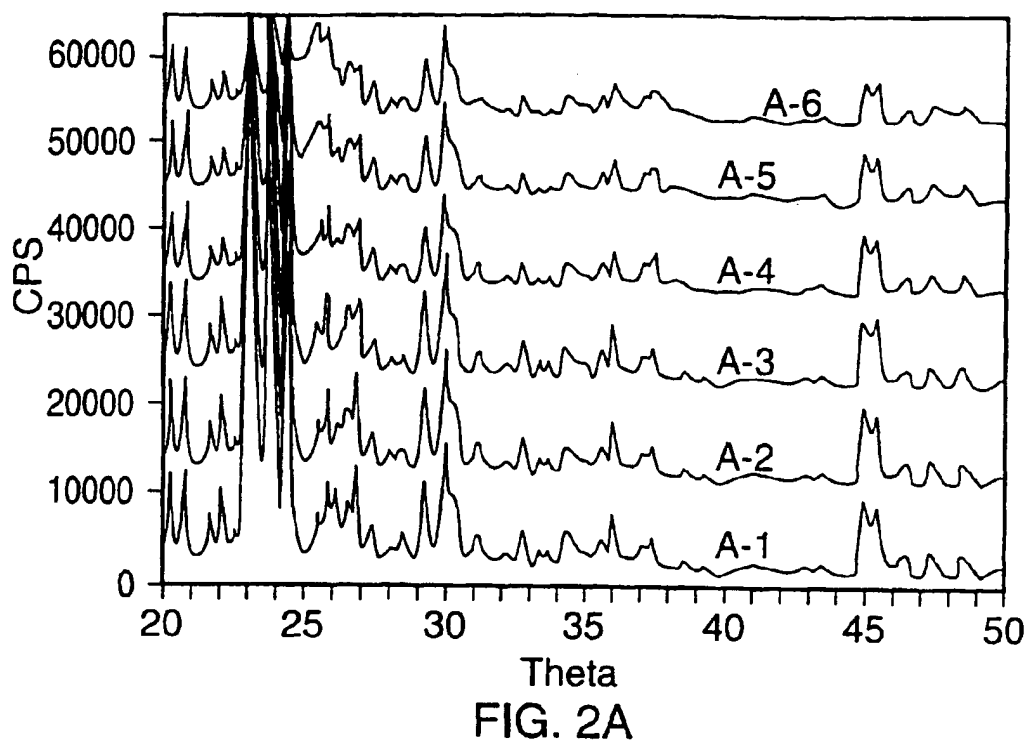
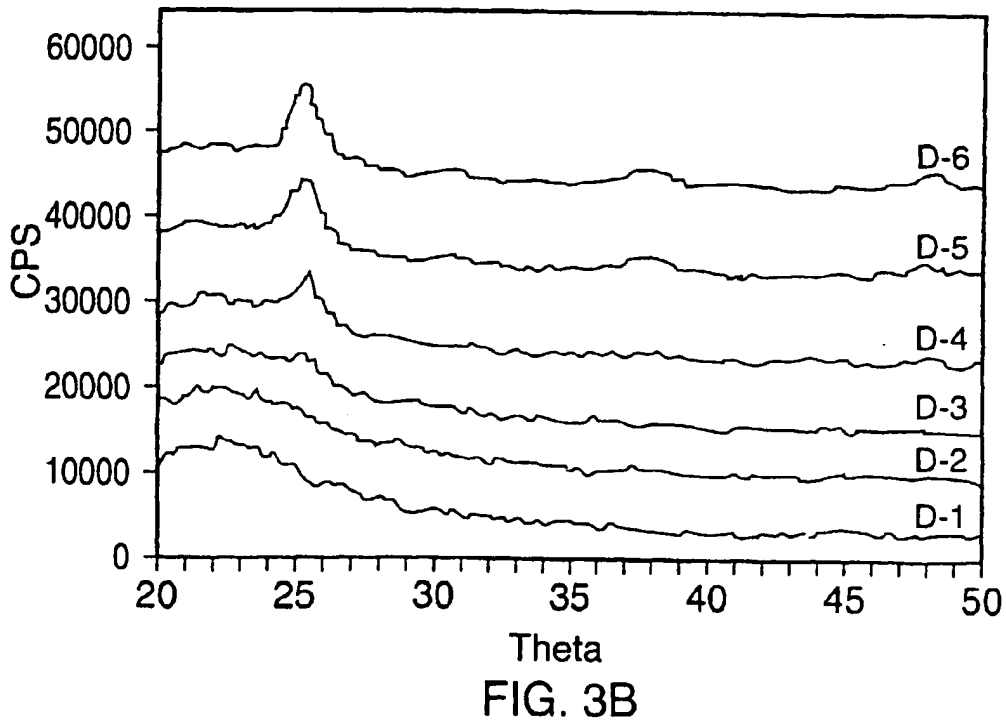
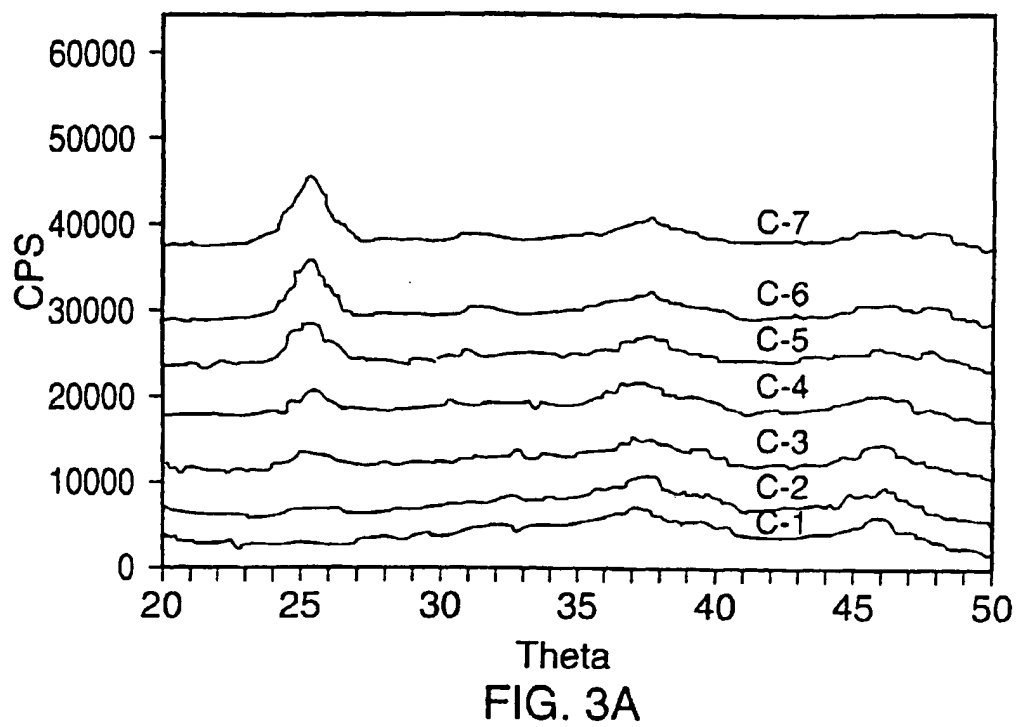


FIG. 1





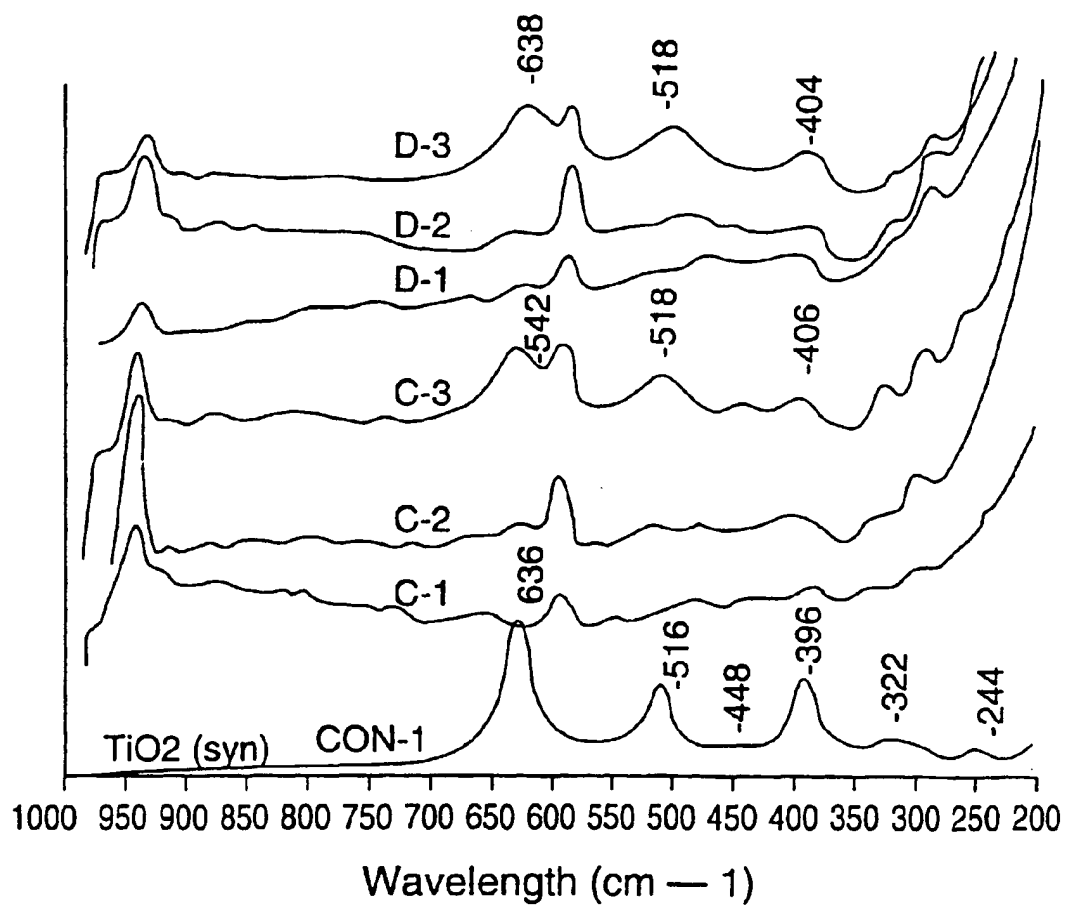


FIG. 4

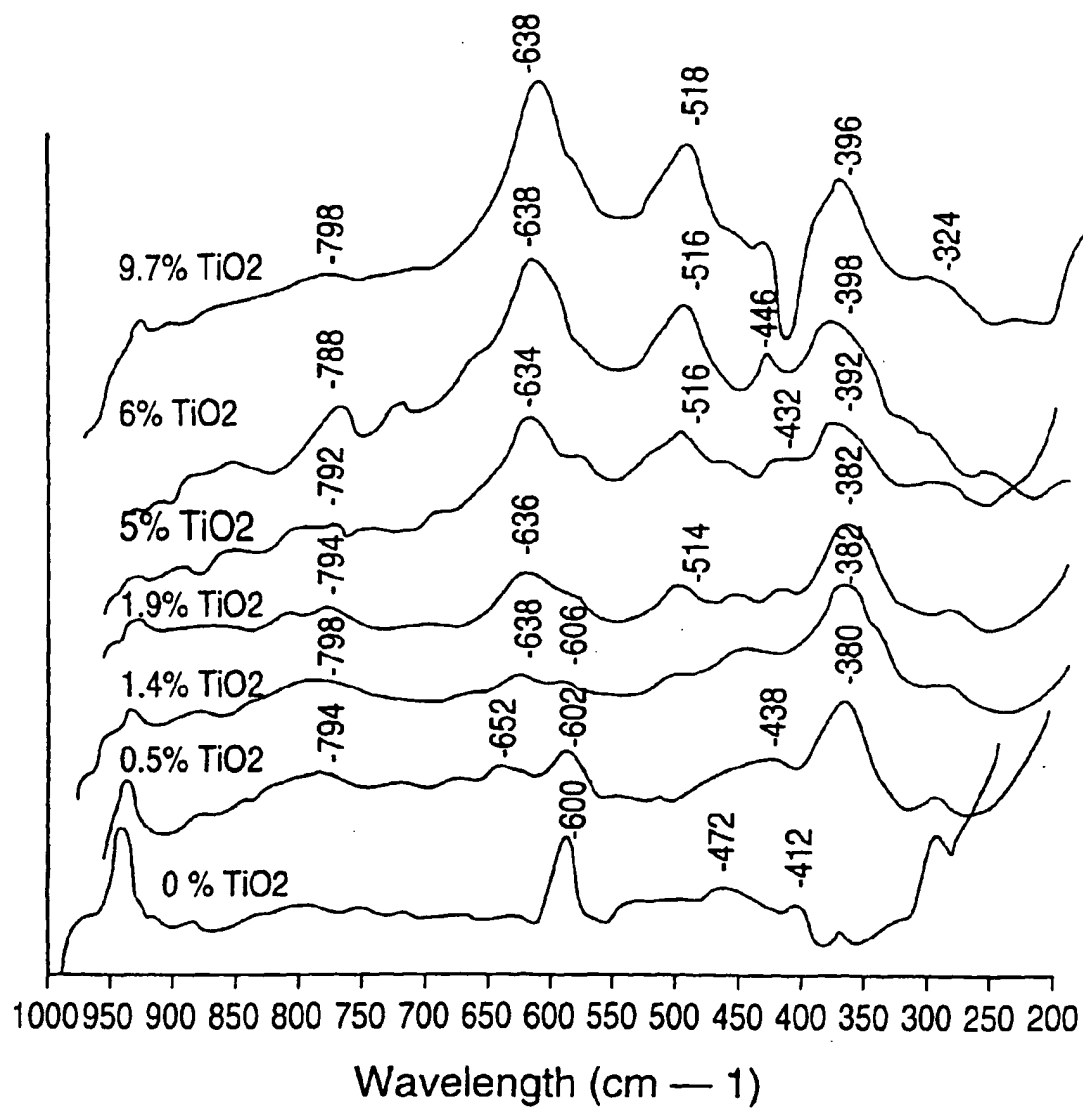


FIG. 5

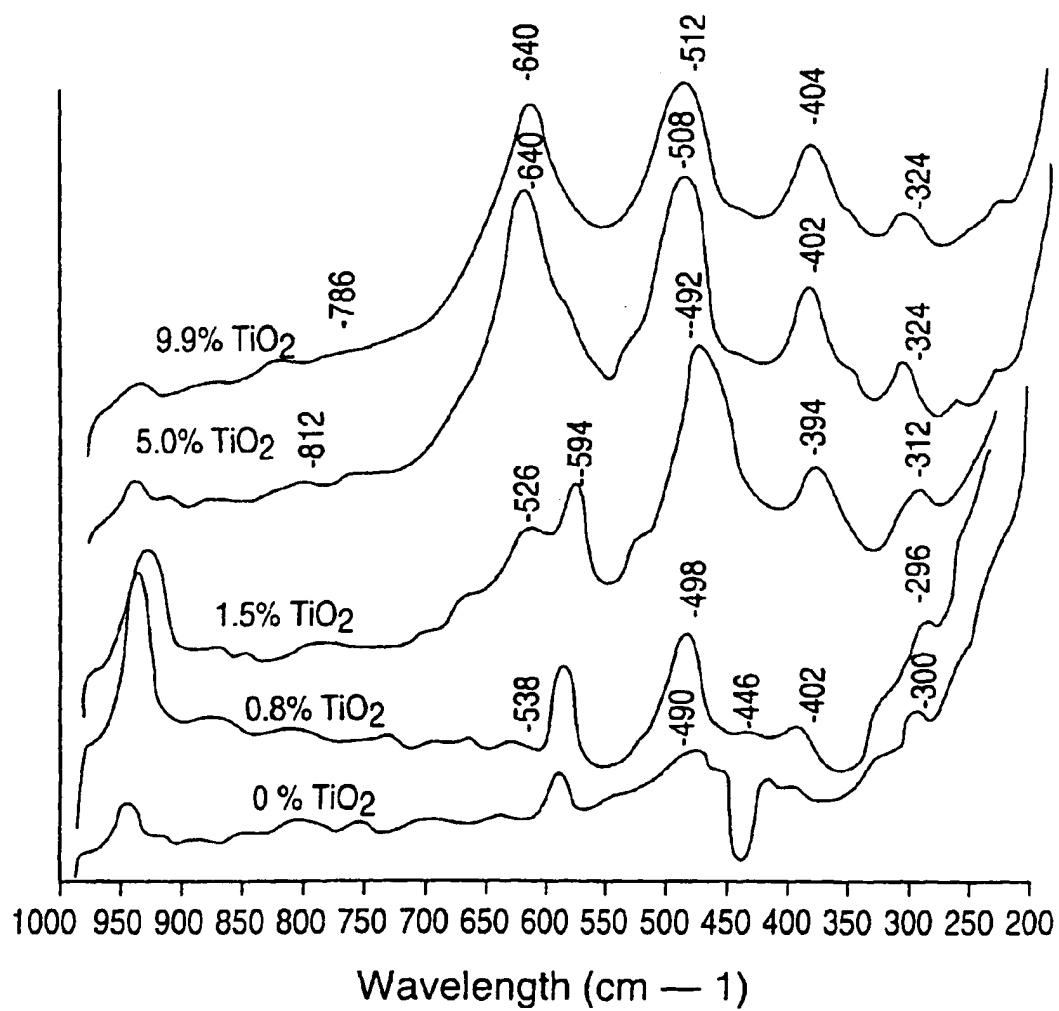


FIG. 6

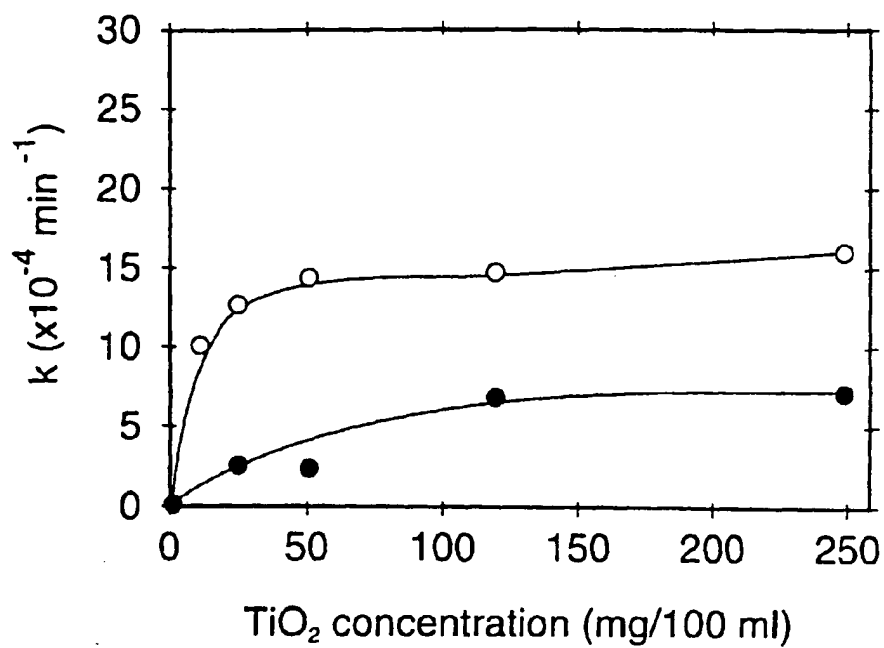


FIG. 7

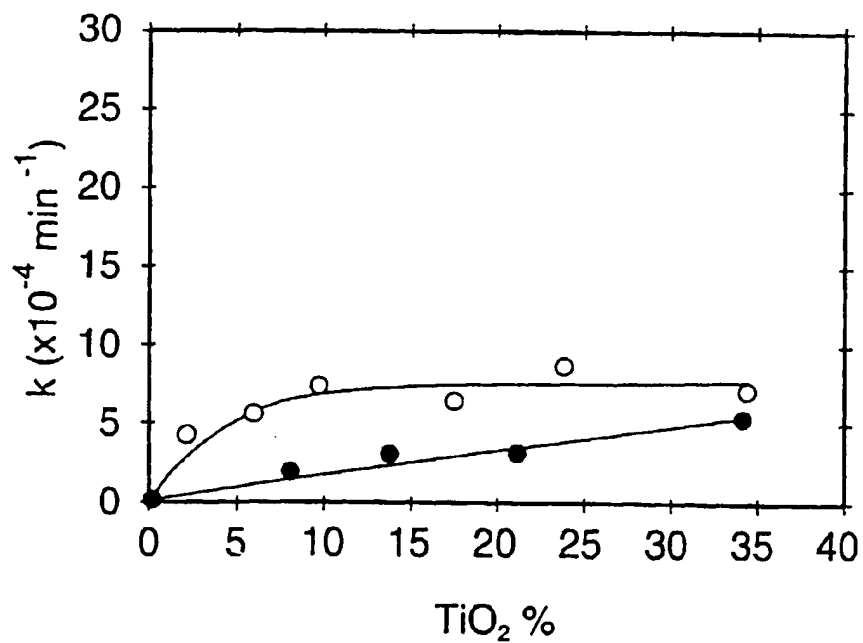


FIG. 8

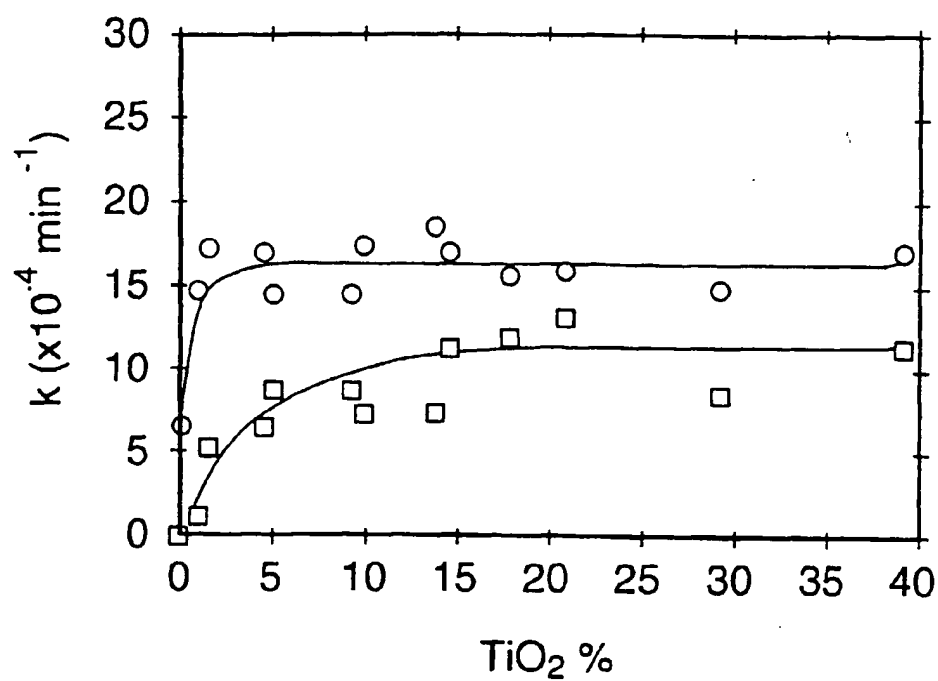


FIG. 9

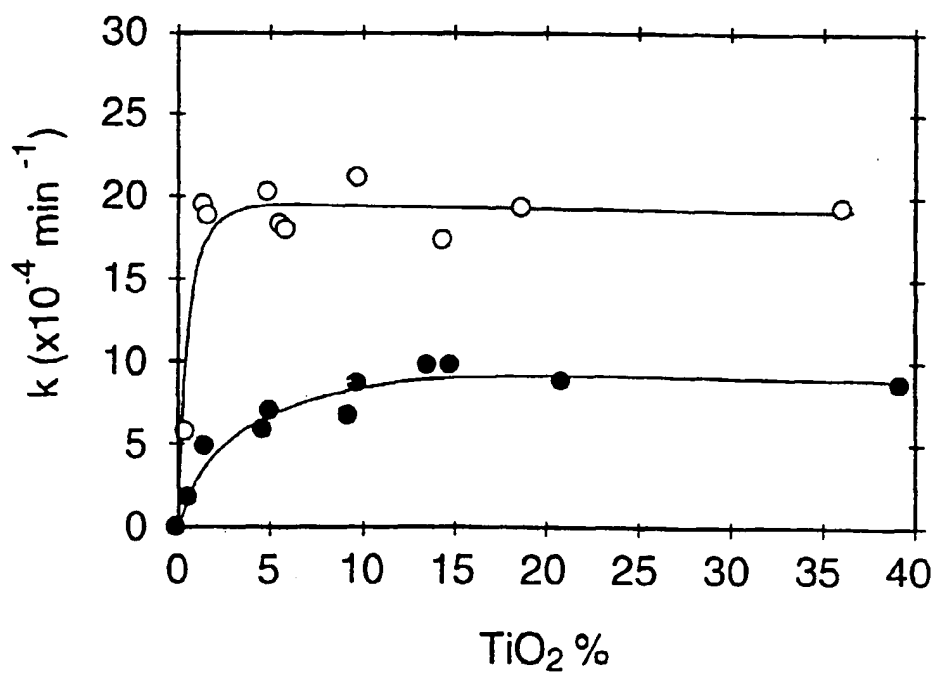


FIG. 10

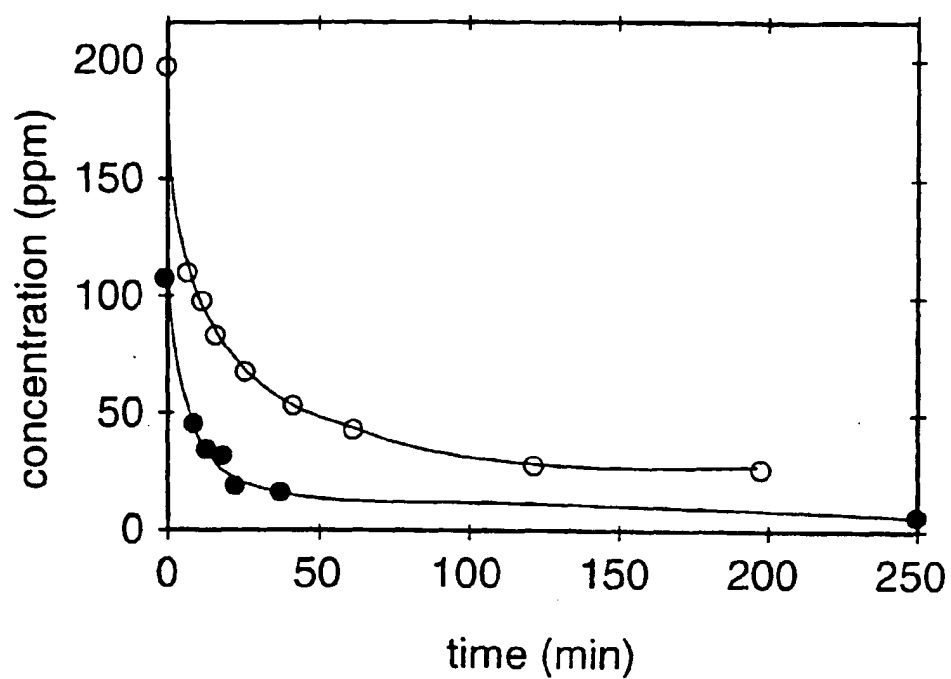


FIG. 11

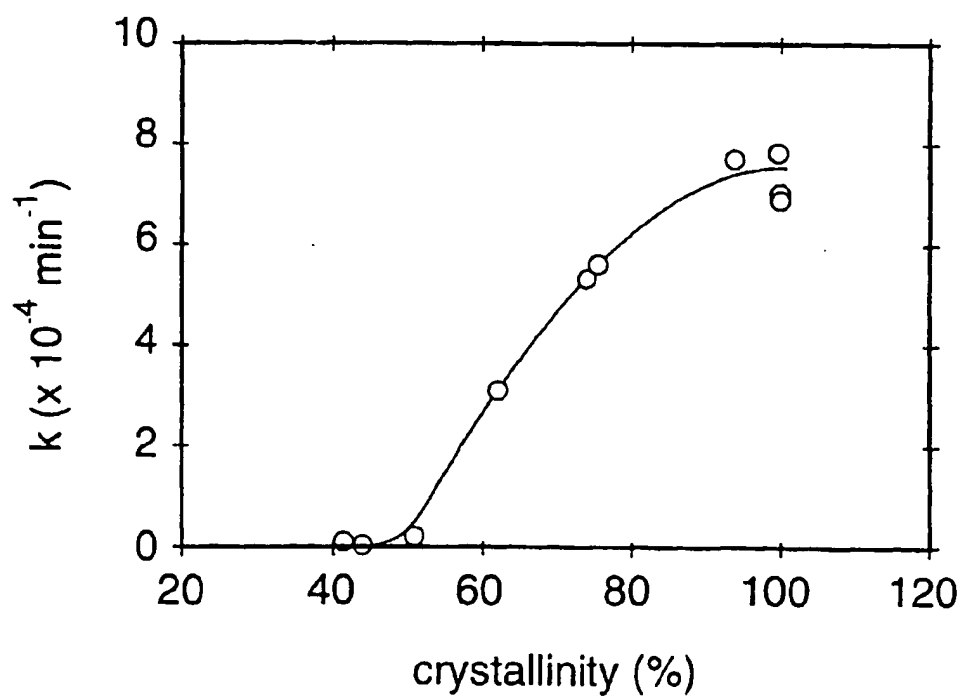


FIG. 12